

Appendix A Thermodynamic Properties of the Ideal-Gas

The molar enthalpy, entropy and Helmholtz free energy of a pure ideal-gas can be expressed according to:

$$H^{\circ}(T) = U_0^{\circ} + (\gamma_0 + R)(T - T_0) + \frac{1}{2}\gamma_1(T^2 - T_0^2) + \frac{1}{3}\gamma_2(T^3 - T_0^3) + \frac{1}{4}\gamma_3(T^4 - T_0^4) \quad (\text{A.1})$$

$$S^{\circ}(T, \rho^{\circ}) = S_0^{\circ} + \gamma_0 \ln\left(\frac{T}{T_0}\right) + \gamma_1(T - T_0) + \frac{1}{2}\gamma_2(T^2 - T_0^2) + \frac{1}{3}\gamma_3(T^3 - T_0^3) + R \ln\left(\frac{\rho_0}{\rho^{\circ}}\right) \quad (\text{A.2})$$

$$A^{\circ}(T, \rho^{\circ}) = U_0^{\circ} - TS_0^{\circ} + \gamma_0 T \left[1 - \frac{T_0}{T} + \ln\left(\frac{T_0}{T}\right) \right] - \frac{1}{2}\gamma_1 T^2 \left[1 - \frac{T_0}{T} \right]^2 - \frac{1}{6}\gamma_2 T^3 \left[1 + 2\left(\frac{T_0}{T}\right)^3 - 3\left(\frac{T_0}{T}\right)^2 \right] - \frac{1}{12}\gamma_3 T^4 \left[1 + 3\left(\frac{T_0}{T}\right)^4 - 3\left(\frac{T_0}{T}\right)^3 \right] + RT \ln\left(\frac{\rho^{\circ}}{\rho_0}\right) \quad (\text{A.3})$$

For an ideal-gas binary mixture, the molar enthalpy, entropy and Helmholtz free energy can be derived from Eqs. (A.1)-(A.3) using the following relations:

$$H^{\circ}(T, x) = xH_1^{\circ}(T) + (1-x)H_2^{\circ}(T) \quad (\text{A.4})$$

$$S^{\circ}(T, \rho^{\circ}, x) = xS_1^{\circ}(T, \rho^{\circ}) + (1-x)S_2^{\circ}(T, \rho^{\circ}) - R \left[x \ln x + (1-x) \ln(1-x) \right] \quad (\text{A.4})$$

$$A^{\circ}(T, \rho^{\circ}, x) = xA_1^{\circ}(T, \rho^{\circ}) + (1-x)A_2^{\circ}(T, \rho^{\circ}) + RT \left[x \ln x + (1-x) \ln(1-x) \right] \quad (\text{A.5})$$

Appendix B: Thermodynamic Properties with GEOS Model

The vapor-liquid phase behavior of a binary system is calculated by the simultaneous salvation of the following equalities:

$$P = P(T, \rho_L, x) \quad (\text{B.1})$$

$$P = P(T, \rho_V, y) \quad (\text{B.2})$$

$$x\varphi_1(T, \rho_L, x) = y\varphi_1(T, \rho_V, y) \quad (\text{B.3})$$

$$(1-x)\varphi_2(T, \rho_L, x) = (1-y)\varphi_2(T, \rho_V, y) \quad (\text{B.4})$$

φ_i represents the fugacity coefficient of compound i ; x and y the liquid and vapor mole compositions of compound 1.

The Compressibility factor is written as:

$$Z = \frac{1}{1 - b\rho} - \frac{a\rho^2}{RT \left[(1 - d\rho)^2 + c\rho^2 \right]} \quad (\text{B.5})$$

The fugacity coefficient of compound i :

$$\ln \varphi_i = -\ln(1 - b\rho) + \frac{b_{n_i}'\rho}{1 - b\rho} + \frac{a}{4RT\delta} \left(\frac{c_{n_i}'}{c} - 2\frac{a_{n_i}'}{a} \right) \ln \left| \frac{1 - \vartheta_1\rho}{1 - \vartheta_2\rho} \right| - \left[d_{n_i}'\rho + \frac{c_{n_i}'(1 - d\rho)}{2c} \right] \frac{a\rho}{RT \left[(1 - d\rho)^2 + c\rho^2 \right]} - \ln Z \quad (\text{B.6})$$

$$a^{res} = -\ln(1 - b\rho) + \frac{a}{2RT\delta} \ln \left| \frac{1 - \vartheta_1\rho}{1 - \vartheta_2\rho} \right| - \ln Z \quad (\text{B.7})$$

$$h^{res} = \frac{Ta_T' - a}{2RT\delta} \ln \left| \frac{1 - \vartheta_1\rho}{1 - \vartheta_2\rho} \right| + (Z - 1) \quad (\text{B.8})$$

The reduced residual molar entropy:

$$s^{res} = \ln(1 - b\rho) + \frac{a_T}{2R\delta} \ln \left| \frac{1 - \mathcal{G}_1\rho}{1 - \mathcal{G}_2\rho} \right| + \ln Z \quad (\text{B.9})$$

The coefficients a, b, c and d are evaluated with Eqs. (32)-(36).

The derivative according to T of the coefficient a can be calculated as follows:

$$a'_T = \left(\frac{\partial a}{\partial T} \right)_{\rho,n} = \sum_i \sum_j x_i x_j \left(\frac{\partial a_{ij}}{\partial T} \right)_{\rho,n} \quad (\text{B.10})$$

$$\left(\frac{\partial a_{ij}}{\partial T} \right)_{\rho,n} = \frac{[1 - k_{ij} + x_i(k_{ij} - k_{ji})]}{2\sqrt{a_i a_j}} \left[a_j \left(\frac{\partial a_i}{\partial T} \right)_{\rho,n} + a_i \left(\frac{\partial a_j}{\partial T} \right)_{\rho,n} \right] \quad (\text{B.11})$$

$$\left(\frac{\partial a_i}{\partial T} \right)_{\rho,n_k} = \Omega_{a_i} \frac{R^2 T_{C_i}^2}{P_{C_i}} 2\alpha(T_r) \left(\frac{d\alpha_i}{dT} \right) \quad (\text{B.12})$$

$$\left(\frac{d\alpha_i}{dT} \right) = \gamma_{1,i} y_{i,T} + \gamma_{2,i} (y_{i,T})^2 + \gamma_{3,i} (y_{i,T})^3; \quad \text{for } T_r \leq 1 \quad (\text{B.13})$$

$$\left(\frac{d\alpha_i}{dT} \right) = \gamma_{1,i} y_{i,T}; \quad \text{for } T_r > 1 \quad (\text{B.14})$$

$$y_{i,T} = \left(\frac{dy_i}{dT} \right) = -\frac{1}{2\sqrt{T_{C_i} T}} \quad (\text{B.15})$$

The derivatives according to the mole fraction n₁ and n₂ of the coefficients a, b, c and d are:

$$a'_{n_1} = \left(\frac{\partial a}{\partial n_1} \right)_{T,\rho,n_2} = 2x_1 a_{11} + x_2 (a_{12} + a_{21}) + 2x_1 x_2^2 (k_{12} - k_{21}) \sqrt{a_1 a_2} \quad (\text{B.16})$$

$$a'_{n_2} = \left(\frac{\partial a}{\partial n_2} \right)_{T,\rho,n_1} = 2x_2 a_{22} + x_1 (a_{12} + a_{21}) + 2x_2 x_1^2 (k_{21} - k_{12}) \sqrt{a_1 a_2} \quad (\text{B.17})$$

$$b'_{n_1} = \left(\frac{\partial b}{\partial n_1} \right)_{T,\rho,n_2} = 2(x_1 b_{11} + x_2 b_{12}) - b \quad (\text{B.18})$$

$$b'_{n_2} = \left(\frac{\partial b}{\partial n_2} \right)_{T,\rho,n_1} = 2(x_1 b_{11} + x_2 b_{12}) - b \quad (\text{B.19})$$

$$c'_{n_1} = \left(\frac{\partial c}{\partial n_1} \right)_{T,\rho,n_2} = 2(x_1 c_{11} + x_2 c_{12}) \quad (\text{B.20})$$

$$c'_{n_2} = \left(\frac{\partial c}{\partial n_1} \right)_{T,\rho,n_2} = 2(x_2 c_{22} + x_1 c_{12}) \quad (\text{B.21})$$

$$d'_{n_1} = \left(\frac{\partial d}{\partial n_1} \right)_{T,\rho,n_2} = d_1 \quad (\text{B.22})$$

$$d'_{n_2} = \left(\frac{\partial d}{\partial n_2} \right)_{T,\rho,n_2} = d_2 \quad (\text{B.23})$$

The quantities δ , \mathcal{G}_1 and \mathcal{G}_2 are calculated according to:

$$\delta = \sqrt{|c|} \quad \mathcal{G}_1 = d - \delta \quad \mathcal{G}_2 = d + \delta \quad (\text{B.24})$$